

## Full Length Article

Co<sub>3</sub>O<sub>4</sub>-FeOOH as a heterojunction electrocatalyst for highly-efficient hydrazine-assisted water electrolysis and pollutant degradation

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## ABSTRACT

The hydrazine oxidation reaction (HzOR) offers a promising alternative to mitigate the high energy demands associated with the kinetically sluggish oxygen evolution reaction. Consequently, developing an efficient electrocatalyst for HzOR is crucial. In this study, we present a highly effective Co<sub>3</sub>O<sub>4</sub>-FeOOH heterojunction designed to enhance hydrazine-assisted water splitting performance. Various characterization techniques were employed to analyze the structures and compositions of the catalyst. Evaluations of its electrocatalytic performance revealed exceptional catalytic activity during hydrazine electrolysis, achieving a current density of 100 mA cm<sup>-2</sup> with a minimal negative potential of -17.2 mV (vs. RHE). The system exhibited impressive stability, maintaining consistent performance for over 100 h during HzOR. Notably, the heterostructure electrocatalyst demonstrated outstanding performance and stability in simulated seawater, requiring only -70 mV (vs. RHE) to deliver a current density of 100 mA cm<sup>-2</sup> and remaining stable after the durability test. The electrocatalyst also performed well in harsh environments, including brine and highly alkaline environments. These findings highlight the potential of the Co<sub>3</sub>O<sub>4</sub>-FeOOH heterostructure electrocatalyst for energy-efficient hydrogen production and pollutant degradation.

## 1. Introduction

The excessive consumption of fossil fuels has led to the emission of massive amounts of greenhouse gases into the atmosphere, contributing to climate change and widespread environmental pollution [1–3]. There is an urgent need for clean, emission-free, and sustainable energy sources as alternatives [4–7]. Hydrogen stands out as an ideal candidate for renewable energy due to its high energy density and emission-free nature during consumption [8–15].

In recent years, electrochemical water splitting has emerged as a promising strategy among various hydrogen production methods [16,17]. This process involves two half-reactions: the hydrogen evolution reaction (HER) at the cathode and the oxygen evolution reaction (OER) at the anode [18]. Compared to HER, OER is a four-electron

transfer process that is kinetically sluggish and requires a high theoretical electrode potential (1.23 V vs RHE), significantly reducing overall conversion efficiency and increasing power consumption, making the water electrolysis process energy-intensive and less favorable from a sustainability standpoint [19–21]. Therefore, anodic electrochemical reactions with lower electrode potentials, such as the oxidation of small molecules like hydrazine, urea, alcohols, sulfones, amines, glucose, and aldehydes, are being explored to replace the energy-intensive OER [8,22].

Among these reactions, the hydrazine oxidation reaction (HzOR, N<sub>2</sub>H<sub>4</sub> + 4OH<sup>-</sup> → N<sub>2</sub> + 4H<sub>2</sub>O + 4e<sup>-</sup>) is extensively studied due to its significantly lower theoretical electrode potential (-0.33 V vs. RHE), which helps mitigate the drawbacks associated with the OER [23,24]. Hydrazine is widely used as a raw chemical in various fields, including

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industry, agriculture, medicine, and dye synthesis [25–27]. However, its extensive application can have adverse effects on environment, ecological balance, agricultural productivity, and may even pose serious risk to human health if not properly managed [28,29]. Once it enters the human body, hydrazine can rapidly induce symptoms such as dizziness, nausea, cough and dyspnea. It can also corrode the skin, causing redness, pain, and even ulceration [27]. The HzOR can serve as a dual purpose by neutralizing hydrazine-containing industrial waste while enabling energy-saving hydrogen production, making it an effective strategy for both pollutant degradation and sustainable energy generation [30]. Therefore, coupling pollutant degradation with hydrogen production is a highly forward-looking endeavour [27,31]. In this context, developing highly efficient electrocatalysts for HzOR is crucial.

Currently, the development of electrocatalysts based on earth-abundant elements (such as Fe, Ni, and Co), including transition metal oxides (TMOs), hydroxides, phosphides, and selenides, is receiving significant attention as a cost-effective strategy for sustainable catalysis [32–35]. TMOs, in particular, have emerged as promising electrocatalysts for anodic electrochemical reactions such as the OER and HzOR, owing to their low cost, earth abundance, and good stability in alkaline media [36–39]. The diverse chemical states of TMOs facilitate efficient charge transfer, crucial for enhancing HzOR performance. Among various TMOs, Co-based oxides like  $\text{Co}_3\text{O}_4$  and their heterostructures have demonstrated good activity due to mixed valence states of Co species ( $\text{Co}^{2+}$  and  $\text{Co}^{3+}$ ), which enhance electron transport and increase the number of active sites [40–42]. High valence cations exhibit strong intrinsic activity toward HzOR, contributing to reduced overpotential and enhanced reaction kinetics [27,42,43]. Moreover, strong interfacial interactions in heterostructures can accelerate charge transfer and optimize the adsorption/desorption behaviors of reaction intermediates, attributed to the electronic coupling between different components [44–48]. Heterostructure engineering is therefore regarded as one of the most promising strategies for improving anodic reaction performance in hydrolysis [49]. Moreover, the hierarchical porous structure of heterostructures offers abundant channels for electrolyte penetration and gas diffusion, thereby facilitating mass transfer [50,51].

In this study, we fabricated a porous  $\text{Co}_3\text{O}_4$ -FeOOH heterojunction on conductive nickel foam (NF), combining the strong adsorption capability of Fe-based oxide/hydroxides for electrocatalytic intermediates with the robust HzOR activity of  $\text{Co}_3\text{O}_4$  [52]. The resulting electrocatalyst exhibited remarkable activity towards HzOR, achieving a low potential of  $-17.2$  mV (vs. RHE) at a current density of  $100 \text{ mA cm}^{-2}$  and requiring only  $122.1$  mV (vs. RHE) to reach  $400 \text{ mA cm}^{-2}$ . The outstanding bifunctional electrocatalytic performance of  $\text{Co}_3\text{O}_4$ -FeOOH heterojunction enables efficient overall hydrazine splitting (OH<sub>2</sub>S). In a two-electrode configuration, a cell voltage of only  $0.49$  V was required to deliver a current density of  $300 \text{ mA cm}^{-2}$ . The electrocatalyst demonstrates remarkable stability, maintaining continuous operation for over  $116$  h at  $100 \text{ mA cm}^{-2}$  in HzOR. The excellent performance of the electrocatalyst can also extends to harsh conditions such as simulated seawater, highly saline environments, and strong alkaline media. More importantly, the electrocatalyst exhibited high degradation efficiency for hydrazine-containing solutions, highlighting its potential for both clean hydrogen production and pollutant elimination.

## 2. Methodology

### 2.1. Materials and chemicals

Cobalt nitrate hexahydrate ( $\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ , 99.9 %) was purchased from Kojundo Chemical Laboratory Co., Ltd. (Japan). Ethanol (EtOH,  $\text{C}_2\text{H}_6\text{O}$ , 99.5 %), acetone ( $\text{C}_3\text{H}_6\text{O}$ , 99.5 %), ferrous chloride tetrahydrate ( $\text{FeCl}_2 \cdot 4\text{H}_2\text{O}$ , 99.0 %), urea ( $\text{CO}(\text{NH}_2)_2$ , 90 %), potassium hydroxide (KOH, 85 %), sodium chloride (NaCl, 90 %), para-dimethylaminobenzaldehyde (PDAB,  $\text{C}_9\text{H}_{11}\text{NO}$ ) and hydrochloric acid (HCl, 30 %) were purchased from FUJIFILM Wako Pure Chemical Co.

(Japan). Hydrazine monohydrate ( $\text{N}_2\text{H}_4 \cdot \text{H}_2\text{O}$ , 98 %) was purchased from Sigma-Aldrich, Ltd. NF was purchased from Goodfellow, Ltd. All reagents used in this study were used without further purification.

### 2.2. Preparation of $\text{Co}_3\text{O}_4$ -FeOOH

The  $\text{Co}_3\text{O}_4$ -FeOOH heterostructure electrocatalyst was prepared via a three-step process, as shown in Fig. 1. Firstly, before the synthesis, a piece of NF was cleaned in  $1.0 \text{ M HCl}$ , acetone, and ethanol subsequently. Then, FeOOH layer was prepared by immersing the cleaned NF in a  $50 \text{ mM FeCl}_2$  solution and putting it into a microwave oven at  $900 \text{ W}$  for one minute. The product was washed with deionized water and ethanol, and dried overnight at  $60^\circ\text{C}$  in a vacuum oven.  $\text{Co}_3\text{O}_4$ -FeOOH was synthesized according to the previous report [53]. In brief,  $1.455 \text{ g}$  of  $\text{Co}(\text{NO}_3)_2$  and  $1.818 \text{ g}$  of urea were dissolved in a mixture containing deionized water and ethyl alcohol in a glass bottle (volume ratio, 1:1,  $100 \text{ mL}$ ) under ultrasonication. After drying, the FeOOH-coated NF was placed in the above solution, sealed with a cap, and heated at  $90^\circ\text{C}$  for  $8 \text{ h}$  in a furnace. The  $\text{Co}_3\text{O}_4$ -FeOOH was obtained by calcining the dried intermediate at  $400^\circ\text{C}$  for  $2 \text{ h}$  in a muffle furnace.

### 2.3. Characterizations

X-ray diffractometer (XRD, Rigaku SmartLab), with Cu Ka radiation source ( $1.5418 \text{ \AA}$ ), was employed to investigate the phases and crystal structures of the electrocatalysts. Scanning electron microscopy (SEM, Thermo Fisher Scientific Helios Hydra CX), with a working voltage of  $10 \text{ kV}$ , was used to examine the morphologies, and the energy-dispersive spectrometry (EDS, Oxford instruments Xplore) was used to investigate the composition. A transmission electron microscope (TEM, Thermo Fisher Talos F200X) was used to further investigate the morphologies and microstructures. X-ray photoelectron spectroscopy (XPS, Shimadzu/KRATOS Corporation AXIS-165) was applied to investigate the surface chemical properties of the samples. The ultraviolet photoelectron spectroscopy (UPS, Thermo Scientific Nexsa, Avantage v.59921) was employed to determine the work function ( $W_f$ ) of the samples, using a He I excitation source ( $h\nu = 21.2 \text{ eV}$ ). A  $-5 \text{ V}$  bias was applied to the samples during the UPS measurement. The value of  $W_f$  was calculated using the photoelectric equation,  $W_f = h\nu - W$ .

### 2.4. Theoretical computation

The crystal structures of  $\text{Co}_3\text{O}_4$  and  $\gamma$ -FeOOH, obtained from the ICDD Powder Diffraction File (PDF 43-1003 for  $\text{Co}_3\text{O}_4$ ; PDF 73-2326 for  $\gamma$ -FeOOH), were fully optimized within density functional theory (DFT) as implemented in the Vienna ab initio simulation package (VASP) [54–56]. The Perdew–Burke–Ernzerhof (PBE) functional [57] was used with a plane-wave basis set and the projector-augmented wave (PAW) method [58]. The on-site Coulomb interaction was treated within the DFT + U framework using Dudarev's approach [59]. For Fe 3d states,  $U = 7.0 \text{ eV}$  and  $J = 1.0 \text{ eV}$  were applied following a previous report [60], while no U correction was applied to the Co 3d states, also in accordance with a prior study [61]. Antiferromagnetic initial spin configurations were assigned for both  $\text{Co}_3\text{O}_4$  and  $\gamma$ -FeOOH based on these previous reports. The plane-wave cutoff energy was set to  $500 \text{ eV}$ . The convergence criterion for the electronic self-consistent field (SCF) loop was set to  $1.0 \times 10^{-5} \text{ eV}$ . Both the atomic positions and cell parameters were fully optimized until the forces on all the atoms became less than  $0.03 \text{ eV}/\text{\AA}$ . The  $\Gamma$ -centered k-point meshes with a k spacing of  $2\pi \times 0.05 \text{ \AA}^{-1}$  were employed for sampling the Brillouin zone. Grimme's D3 dispersion correction formalism with Becke–Johnson damping (D3BJ) [62,63] was adopted. Optimized structures shown in this paper were drawn by using VESTA [64]. Slab models of the  $\text{Co}_3\text{O}_4$  (440) and  $\gamma$ -FeOOH (020) surfaces were generated from the optimized bulk structures using the method developed by Hinuma et al. [65–67]. Each slab was constructed with a thickness of approximately  $8 \text{ \AA}$  and a vacuum layer of about  $15 \text{ \AA}$ .

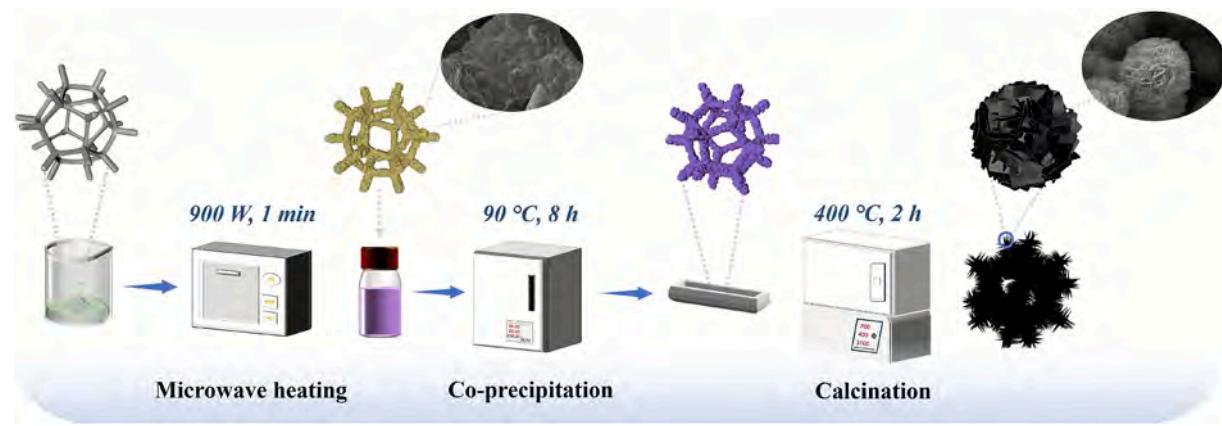


Fig. 1. Schematic illustration of the synthesis of  $\text{Co}_3\text{O}_4$ -FeOOH on NF.

to avoid spurious interactions between periodic images. Among the possible lattice-matching configurations generated using the Interface Builder in QuantumATK, the  $\text{Co}_3\text{O}_4$  (440)/ $\gamma$ -FeOOH (020) interface with a mean absolute strain of 0.96 % was selected. To explore possible atomic arrangements at the interface, one of the slabs was laterally translated parallel to the interface plane, generating twelve distinct  $\text{Co}_3\text{O}_4$  (440)/ $\gamma$ -FeOOH (020) interface configurations. To obtain the most stable interfacial configuration, all twelve  $\text{Co}_3\text{O}_4$  (440)/ $\gamma$ -FeOOH (020) interface models were optimized using the Preferred Potential (PFP) version v7.0.0, a universal Neural Network Potential (NNP) provided by Matlantis Inc [68,69]. The optimization was performed using the Limited-memory Broyden–Fletcher–Goldfarb–Shanno (L-BFGS) method [70] with a convergence threshold of  $1.0 \times 10^{-4}$  eV/Å, applying the ExpCellFilter to allow full relaxation of both atomic positions and the cell parameters. The CRYSTAL\_PLUS\_D3 mode was adopted to include dispersion effects via the D3BJ correction. With the Becke–Johnson damping function. The most stable interface structure obtained from the NNP calculations was further optimized using VASP. The computational parameters were identical to those employed for the individual bulk structure optimizations described above. For the optimized interface structure, the charge density difference and Bader charge analyses [71–74] were performed to investigate the charge redistribution and interfacial charge transfer characteristics.

## 2.5. Electrochemical measurements

The electrocatalytic performance was evaluated using the conventional three-electrode system. A carbon rod and a saturated calomel electrode were employed as the counter and reference electrodes, respectively. The electrolyte was 0.5 M  $\text{N}_2\text{H}_4$  + 1 M KOH for HzOR, while 1 M KOH was used for the OER. All the electrochemical tests were carried out using an electrochemical workstation (Gamry 1010E, USA). The linear sweep voltammetry (LSV) curves were obtained with a scanning rate of  $10 \text{ mV s}^{-1}$ , and were calibrated with iR compensation in the electrochemical workstation. The electrochemical impedance spectroscopy (EIS) was performed at 100 mV throughout a frequency range of 100 kHz to 0.01 Hz. All the potentials obtained were converted to the potentials vs. reversible hydrogen electrode (RHE) using the Nernst equation:

$$E_{\text{RHE}} = E_{\text{Hg/HgO}} - 0.059 \times \text{pH} + E_{\text{Hg/HgO}}^0 \quad (1)$$

where  $E_{\text{Hg/HgO}}^0$  is 98 mV. The Tafel relationship was derived from the LSV curve, and the simplified Butler–Volmer formula was applied to represent it:

$$\eta = a + b \times \log|j| \quad (2)$$

where  $\eta$  represents overpotential,  $a = -b \times \log j_0$ ,  $j_0$  is exchange current

density,  $j$  is current density, and  $b$  represents Tafel slope.

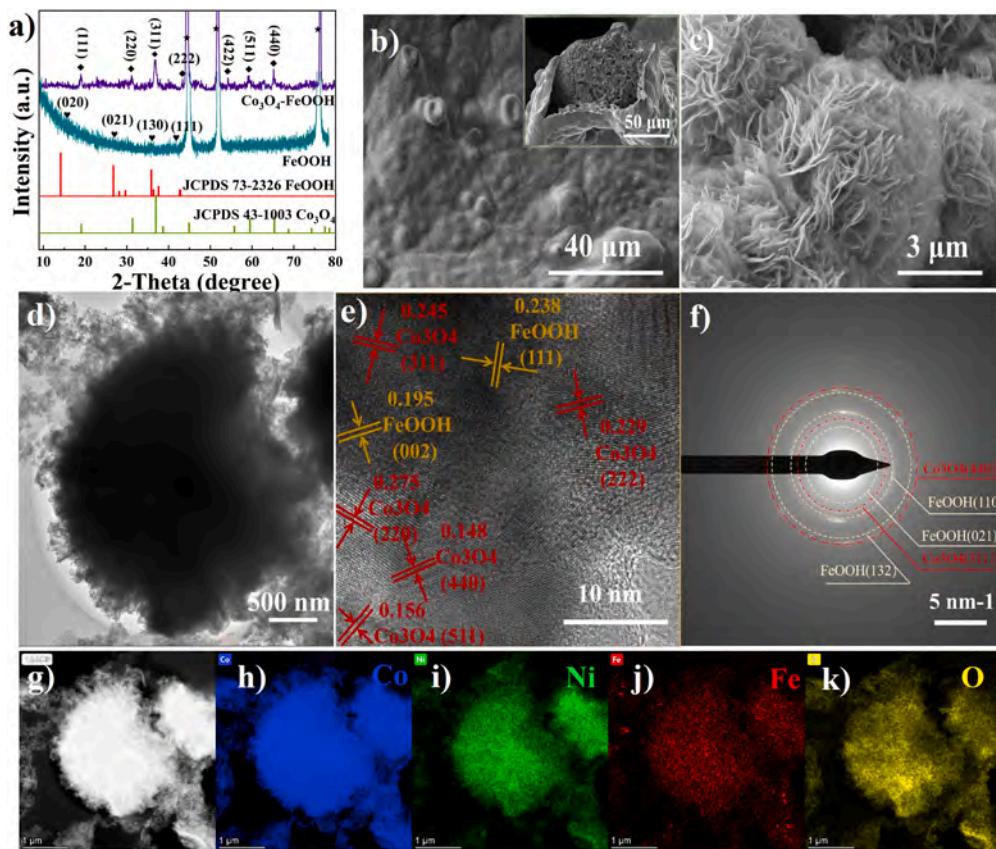
## 2.6. Hydrazine degradation behavior examination

The hydrazine degradation rate was estimated via spectrophotometry [30]. During hydrazine electrolysis, 1 mL of electrolyte was extracted every 20 min to measure the absorbance of  $\text{N}_2\text{H}_4$ , using an ultraviolet–visible spectrophotometer at 458 nm. Under acidic conditions,  $\text{N}_2\text{H}_4$  reacts with PDAB to form a stable-colored complex, enabling the concentration of  $\text{N}_2\text{H}_4$  to be determined indirectly by measuring the absorbance of the complex. The acidic condition was created by adding 0.12 M of HCl to the extracted electrolyte. The concentration of  $\text{N}_2\text{H}_4$  at a certain interval was determined from the obtained calibration curve, shown in Fig. S1.

## 3. Results and discussion

To confirm the successful synthesis of the heterostructure, the crystal structure of the samples was studied by XRD. The XRD patterns in Fig. 2a show that FeOOH was successfully synthesized on NF (JSPDS No. 73-2326), and  $\text{Co}_3\text{O}_4$  was synthesized on the  $\gamma$ -FeOOH layer (JSPDS No. 43-1003). The diffraction peaks observed at  $2\theta = 14.64^\circ, 26.71^\circ, 35.20^\circ$ , and  $41.31^\circ$  correspond to the (0 2 0), (0 2 1), (1 3 0), and (1 1 1) facets of  $\gamma$ -FeOOH, respectively, while the weak signal intensities indicate its low crystallinity [75]. No obvious diffraction peaks originating from other impurity phases, such as  $\text{FeO}$ ,  $\text{Fe}_2\text{O}_3$ , and  $\text{Fe}_3\text{O}_4$ , were observed, indicating the successful preparation of phase-pure FeOOH product by the microwave treatment. The diffraction peaks located at  $19.0^\circ, 31.27^\circ, 36.84^\circ, 43.31^\circ, 54.24^\circ, 59.02^\circ$  and  $65.23^\circ$  can be assigned to (1 1 1), (2 2 0), (3 1 1), (2 2 2), (4 2 2), (5 1 1) and (4 4 0) lattice planes of  $\text{Co}_3\text{O}_4$ , respectively. The as-prepared  $\text{Co}_3\text{O}_4$  was identified as a cubic spinel phase with space group Fd3m, which shows fine crystallization [76,77]. The results match well with the observation by TEM-Selected area electron diffraction (SAED, discuss later).

The morphologies of the samples were observed by SEM. In Fig. 2b, the FeOOH sample shows a rough surface, indicating that the iron oxide-hydroxide layer was grown on the NF during the microwave treatment. After  $\text{Co}_3\text{O}_4$  deposition, globe-flower-shaped particles, with an average size of about 6  $\mu\text{m}$ , were observed (Fig. 2c). The flower-like particles, composed of interconnected nanosheets, significantly increase the specific surface area. This unique structure provides abundant adsorption sites, which enhance  $\text{N}_2\text{H}_4$  interaction, promote the activation and adsorption of intermediates, and improve mass transport efficiency during electrochemical processes. The contact angle (CA) measurement further demonstrates that the growth of  $\text{Co}_3\text{O}_4$  on the FeOOH layer enhances the surface hydrophilicity. As shown in Fig. S2, the  $\text{Co}_3\text{O}_4$ -FeOOH exhibits a CA of 0 degrees, indicating complete wettability. In contrast, pure FeOOH shows a CA of 89.7 degrees, reflecting its



**Fig. 2.** a) XRD patterns of various samples; b) SEM images of FeOOH layer, and c) Co<sub>3</sub>O<sub>4</sub>-FeOOH; d) TEM image, e) HRTEM image, f) SAED pattern, g) HAADF image, and h-k) the corresponding element distribution of Co<sub>3</sub>O<sub>4</sub>-FeOOH.

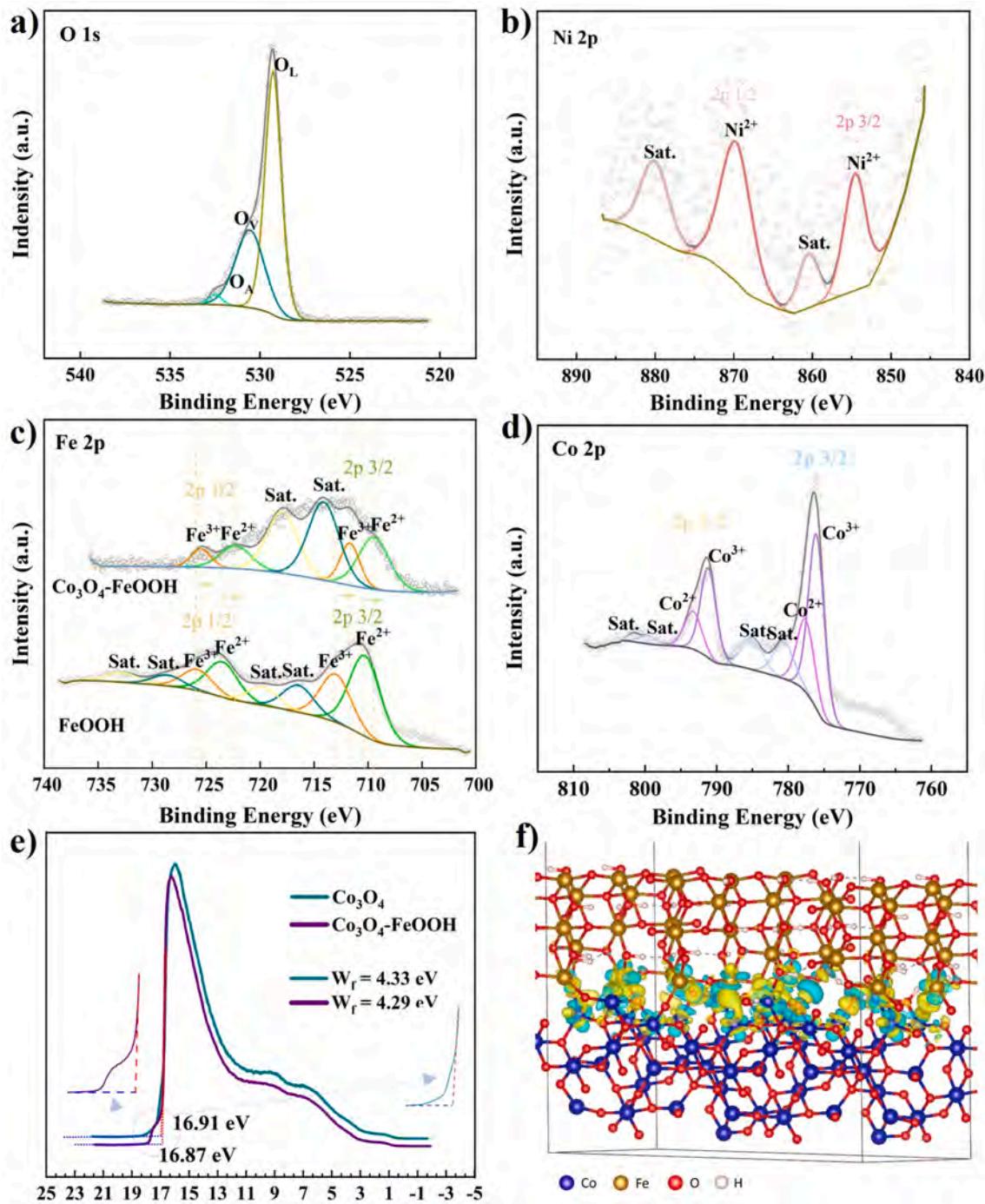
relatively poor hydrophilicity. Pure Co<sub>3</sub>O<sub>4</sub> also displays a CA of 0 degrees, suggesting that the excellent hydrophilicity of the heterostructure primarily originates from the surface morphology and microstructure contributed by the surface Co<sub>3</sub>O<sub>4</sub> layer.

TEM image (Fig. 2d) shows that the morphology of Co<sub>3</sub>O<sub>4</sub>-FeOOH matches well with the SEM observation. The high-resolution transmission electron microscopy (HRTEM) image in Fig. 2e exhibits the multiple interfaces of FeOOH and Co<sub>3</sub>O<sub>4</sub>. The clear lattice fringes with spacing of 0.245 nm, 0.229 nm, 0.275 nm, 0.156 nm, and 0.148 nm are found and can be assigned to (3 1 1), (2 2 2), (2 2 0), (5 1 1), and (4 4 0) planes of Co<sub>3</sub>O<sub>4</sub>. Another set of well-defined lattice fringes with interplanar distances of 0.238 nm and 0.159 nm can be ascribed to the (1 1 1) and (0 0 2) planes of FeOOH. The co-existence of two phases confirmed the heterostructure formation, which is further confirmed by the SAED patterns displayed in Fig. 2f. The diffraction rings associated with the (4 4 0), and (3 1 1) planes of Co<sub>3</sub>O<sub>4</sub>, and (1 1 0), (0 2 1), and (1 3 2) planes of FeOOH were observed. The multiple rings assembled with bright spots in the SAED pattern also demonstrated the polycrystalline nature of the sample. High-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM) image and the corresponding elements distribution mappings (Fig. 2g-k) represent the distribution of Fe, Co, Ni, and O on the electrocatalyst surface, implying the successful formation of Co<sub>3</sub>O<sub>4</sub>-FeOOH/NF heterojunction catalyst.

XPS analysis was conducted to examine the surface chemical environment of the heterojunction electrocatalyst. The full-survey XPS spectrum displayed in Fig. S3 indicates the existence of Co, Fe, O, and Ni in the electrocatalyst. The O 1s spectrum can be deconvoluted into three peaks, located at 529.2, 531.8, and 533.1 eV, which can correspond to the lattice oxygen, oxygen vacancy, and adsorbed oxygen, respectively, as shown in Fig. 3a. The existence of the oxygen vacancies on the catalyst surface enhances the electrocatalytic reaction activity [78]. As

shown in the Ni 2p core level XPS spectrum in Fig. 3b, the Ni 2p<sub>3/2</sub> and the Ni 2p<sub>1/2</sub> peaks, together with their corresponding satellite features associated with Ni<sup>2+</sup> species, indicate the oxidation state of Ni on the surface. However, the weak peak intensities indicate that only a minor amount of Ni exists in the samples. In Fe 2p spectra, the peaks at 709.58 and 729.3 eV ( $\Delta BE = 18.9$  eV) can be ascribed to Fe 2p<sub>3/2</sub> and Fe 2p<sub>1/2</sub> [79]. Deconvoluted peaks at 710.5, 722.5, 711.68, and 726.02 eV, correspond to the 2p<sub>3/2</sub>, and the 2p<sub>1/2</sub> of Fe<sup>2+</sup> and the 2p<sub>3/2</sub>, the 2p<sub>1/2</sub> of Fe<sup>3+</sup> in Co<sub>3</sub>O<sub>4</sub>-FeOOH, and the peaks at 710.48, 723.7, 714.3, and 726.08 eV, corresponding to the 2p<sub>3/2</sub>, and the 2p<sub>1/2</sub> of Fe<sup>2+</sup>, and the 2p<sub>3/2</sub>, and the 2p<sub>1/2</sub> of Fe<sup>3+</sup> in FeOOH, showing a negative shift in binding energy after Co<sub>3</sub>O<sub>4</sub> deposition, as shown in Fig. 3c [80,81]. In the high-resolution Co 2p XPS spectrum (Fig. 3d), the peaks located at 776.3 and 792.5 eV ( $\Delta BE = 16.2$  eV) are associated with the Co 2p<sub>3/2</sub> and the Co 2p<sub>1/2</sub>, respectively. The peaks at 775.1 and 791.0 eV can be assigned to the 2p<sub>3/2</sub> and the 2p<sub>1/2</sub> of Co<sup>3+</sup>, while the peaks at 777.68 and 793.38 eV can be assigned to the 2p<sub>3/2</sub> and the 2p<sub>1/2</sub> of Co<sup>2+</sup> [82]. In contrast to pristine FeOOH, the Fe 2p peaks in Co<sub>3</sub>O<sub>4</sub>-FeOOH shift to lower binding energies, indicating a redistribution of electron density between Co<sub>3</sub>O<sub>4</sub> and FeOOH, owing to the difference in Fermi levels. This suggests successfully formation of an electronically coupled interface between FeOOH and Co<sub>3</sub>O<sub>4</sub> [28,83]. By comparing the calculated Co<sup>3+</sup>/Co<sup>2+</sup> ratios of pure Co<sub>3</sub>O<sub>4</sub> (Fig. S4) and Co<sub>3</sub>O<sub>4</sub>-FeOOH, the heterojunction exhibits a slightly higher ratio than the pure material, further supporting the presence of charge transfer between Co<sub>3</sub>O<sub>4</sub> and FeOOH, within the heterojunction. This interfacial charge redistribution promotes electronic structure modulation and accelerates the reaction kinetics.

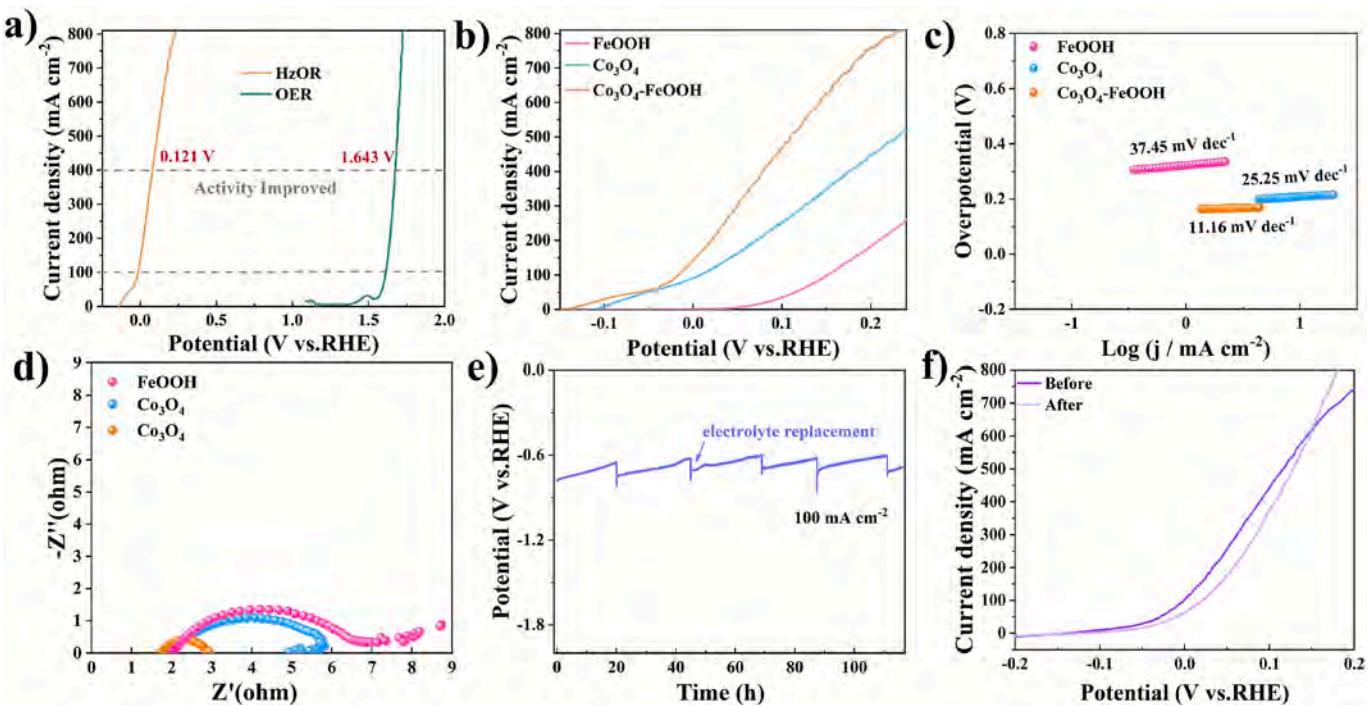
UPS was employed to investigate the electronic properties of the heterojunction [84]. The calculated W<sub>f</sub> of Co<sub>3</sub>O<sub>4</sub>, and Co<sub>3</sub>O<sub>4</sub>-FeOOH are 4.33 eV, and 4.29 eV, respectively. The decrease in W<sub>f</sub> after Co<sub>3</sub>O<sub>4</sub> comes



**Fig. 3.** Core level spectra of a) O 1s; b) Ni 2p, c) Fe 2p, and d) Co 2p of  $\text{Co}_3\text{O}_4$ -FeOOH; e) UPS spectrum of  $\text{Co}_3\text{O}_4$ , and  $\text{Co}_3\text{O}_4$ -FeOOH; f) Charge-density difference ( $0.005 \text{ bohr}^{-3}$  isosurface; yellow = charge accumulation, blue = charge depletion) for the  $\text{Co}_3\text{O}_4$ (440)/ $\gamma$ -FeOOH(020) interface.

into contact with the FeOOH layer indicates interfacial electron transfer between  $\text{Co}_3\text{O}_4$  and FeOOH, as shown in Fig. 3e. Theoretical calculation also verified the formation of this interfacial electronic field. As shown in Fig. 3f, the charge-density difference for the optimized  $\text{Co}_3\text{O}_4$ (440)/ $\gamma$ -FeOOH(020) interface reveals pronounced electron redistribution concentrated at the Fe–O–Co linkages and at interfacial H bonds formed between Fe–OH and Co–OH groups. These features indicate strong interfacial interactions and an electronically coupled interface, leading to a modulation of the local electronic structure. Consistently, Bader analysis yields a net charge of  $-0.16 \text{ |e|}$  on the  $\gamma$ -FeOOH slab and  $+0.16 \text{ |e|}$  on the  $\text{Co}_3\text{O}_4$  slab, confirming charge transfer from  $\text{Co}_3\text{O}_4$  to  $\gamma$ -FeOOH.

LSV was carried out to evaluate the performance of  $\text{Co}_3\text{O}_4$ -FeOOH towards HzOR and OER, shown in Fig. 4a, where the electrolyte was  $0.5 \text{ M } \text{N}_2\text{H}_4 + 1 \text{ M KOH}$  in the HzOR, while being  $1 \text{ M KOH}$  in the OER. The  $\text{Co}_3\text{O}_4$ -FeOOH electrocatalyst exhibits a remarkable catalytic activity toward the HzOR, enabling low working potential in hydrazine-assisted electrolysis compared to the much higher voltages required for the OER. A small negative potential of  $-17.2 \text{ mV}$  (vs. RHE) is sufficient to drive a current density of  $100 \text{ mA cm}^{-2}$ , significantly lower than that required for the OER ( $1.583 \text{ V}$ , vs. RHE), indicating a substantially reduced energy input, surpassing previously reported studies (Table S1). In addition, a high current density of  $400 \text{ mA cm}^{-2}$  was delivered at  $122.1 \text{ mV}$  (vs. RHE), demonstrating the potential for substantial energy savings at



**Fig. 4.** a) Performances of  $\text{Co}_3\text{O}_4$ -FeOOH in HzOR (1 M KOH + 0.5 M  $\text{N}_2\text{H}_4$ ) and OER (1 M KOH); b) LSV curves of  $\text{Co}_3\text{O}_4$ -FeOOH,  $\text{Co}_3\text{O}_4$ , and  $\text{FeOOH}$  during HzOR; c) Tafel slopes derives from LSVs; d) EIS curves of  $\text{Co}_3\text{O}_4$ -FeOOH,  $\text{Co}_3\text{O}_4$ , and  $\text{FeOOH}$  in HzOR; e) Stability test of  $\text{Co}_3\text{O}_4$ -FeOOH in HzOR, and f) LSV curves of  $\text{Co}_3\text{O}_4$ -FeOOH before and after stability test.

higher current density operation. To demonstrate the superior catalytic activity of  $\text{Co}_3\text{O}_4$ -FeOOH heterojunction, the HzOR performances of the constituting components,  $\text{Co}_3\text{O}_4$  and  $\text{FeOOH}$ , were also examined under the same conditions. As shown in Fig. 4b, at a current density of 200  $\text{mA cm}^{-2}$ , the  $\text{Co}_3\text{O}_4$ -FeOOH exhibits a notable catalytic activity with a low potential of 20 mV (vs. RHE), which is significantly lower than that of the potential of  $\text{Co}_3\text{O}_4$  (72 mV, vs. RHE) and  $\text{FeOOH}$  (210 mV, vs. RHE). The result further indicates that the  $\text{Co}_3\text{O}_4$  is the primary active component for the HzOR. Tafel plots were derived from the LSV polarization curves to investigate the electrochemical kinetics of the HzOR. As shown in Fig. 4c, the Tafel slope of  $\text{Co}_3\text{O}_4$ -FeOOH ( $11.16 \text{ mV dec}^{-1}$ ) is much smaller than that of  $\text{FeOOH}$  ( $37.45 \text{ mV dec}^{-1}$ ), and slightly lower than that of  $\text{Co}_3\text{O}_4$  ( $25.25 \text{ mV dec}^{-1}$ ), proving the favorable catalytic kinetics towards HzOR of the heterojunction. The reaction kinetics were further assessed by electrochemical impedance spectroscopy (EIS). From the Nyquist curves in Fig. 4d,  $\text{Co}_3\text{O}_4$ -FeOOH has a much smaller semi-circle radius than that of the  $\text{Co}_3\text{O}_4$  and  $\text{FeOOH}$ , indicating a much lower electrode-transfer-resistance ( $R_{ct}$ ) and thus a higher charge-transfer rate and more rapid catalytic kinetics [85,86]. The result indicates that the electron migration is accelerated by the enhanced interaction between the  $\text{Co}_3\text{O}_4$  and  $\text{FeOOH}$  after  $\text{Co}_3\text{O}_4$  deposition on  $\text{FeOOH}$ , which improves the electron-transfer capacity of the catalyst [87].

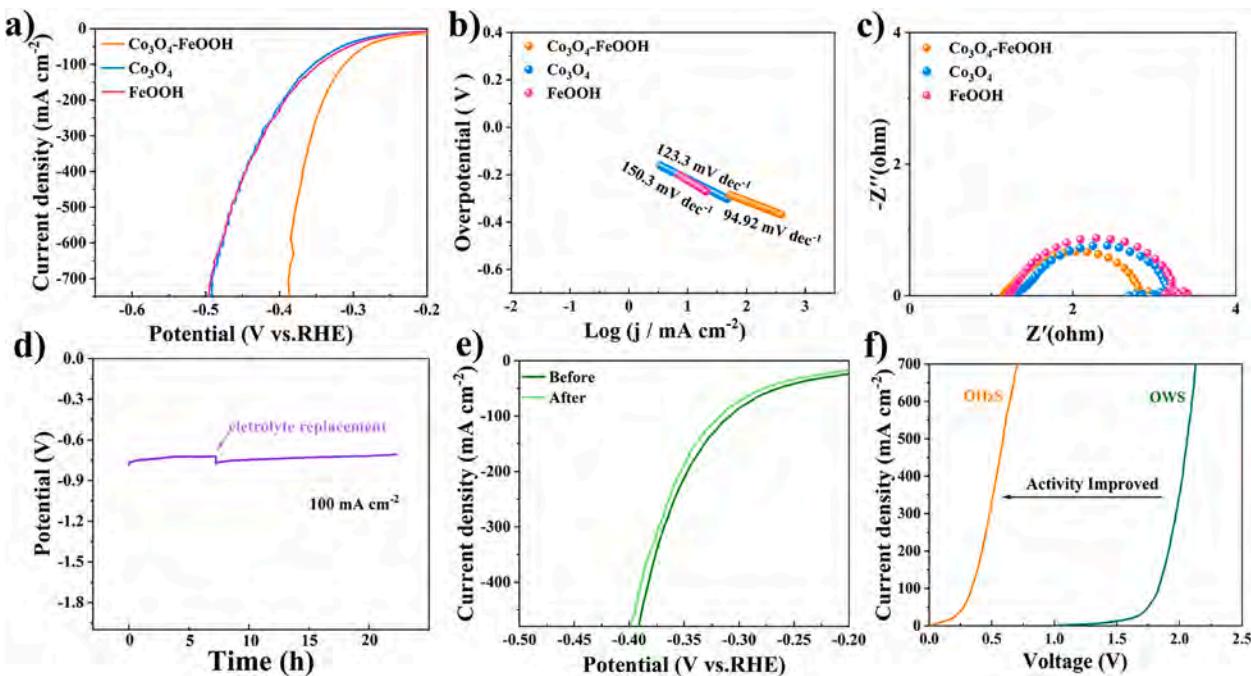
The long-term stability of the heterostructure electrocatalyst was examined by chronopotentiometry (CP) test. The CP curve in Fig. 4e shows that the potential remains stable for more than 116 h at a current density of 100  $\text{mA cm}^{-2}$ . The LSV polarization curve was measured again (Fig. 4f) after the CP test, which shows negligible attenuation. The structure and valence state changes of the catalyst after stability test were also investigated, and the results are shown in Fig. S5. SEM analysis of the post-CP-test electrocatalyst (Fig. S5a) shows some morphological transformation, with the ball-shaped particles becoming smaller. Comparing the EDS data with the pre-reaction state (Fig. S5b, Fig. S6, Table S2), no significant changes in the Fe, Co and O ratio were observed, indicating that no noticeable outward diffusion occurred. In contrast, the  $\text{Co}^{2+}/\text{Co}^{3+}$  and  $\text{Fe}^{2+}/\text{Fe}^{3+}$  ratios increased, implying that both  $\text{Co}^{3+}$  and  $\text{Fe}^{3+}$  in the  $\text{Co}_3\text{O}_4$ -FeOOH heterojunction participated in

the oxidation of  $\text{N}_2\text{H}_4$  throughout the reaction.

Cyclic voltammetry (CVs) were used to quantify the electrochemical surface area, and double layer capacitance ( $C_{dl}$ ). The effective electrochemically active surface area (ECSA) can be calculated using the equation:  $ECSA = C_{dl}/C_s$ , where  $C_s$  is the specific capacitance. The  $C_{dl}$  value was evaluated from the CVs recorded at different scan rates (Fig. S7), and the results are shown in Fig. S8. The  $\text{Co}_3\text{O}_4$ -FeOOH sample exhibits a much larger  $C_{dl}$  ( $12.16 \text{ mF cm}^{-2}$ ) than that of the  $\text{FeOOH}$  ( $4.42 \text{ mF cm}^{-2}$ ), indicating that  $\text{Co}_3\text{O}_4$ -FeOOH possesses a higher ECSA than  $\text{FeOOH}$ . This demonstrates that the heterojunction electrocatalyst provides more accessible catalytic sites and achieves higher atomic utilization efficiency towards HzOR.

The HER activities of  $\text{Co}_3\text{O}_4$ -FeOOH,  $\text{Co}_3\text{O}_4$ , and  $\text{FeOOH}$  were also evaluated in the electrolyte, which consisted of 1 M KOH and 0.5 M  $\text{N}_2\text{H}_4$ . As shown in Fig. 5a,  $\text{Co}_3\text{O}_4$ -FeOOH requires a potential of  $-358 \text{ mV}$  (vs. RHE) to deliver a current density of  $-200 \text{ mA cm}^{-2}$ , while  $\text{Co}_3\text{O}_4$  and  $\text{FeOOH}$  require  $-402 \text{ mV}$  (vs. RHE) and  $-398 \text{ mV}$  (vs. RHE) to deliver the same current density, respectively. The HER performance of the heterojunction catalyst is better than that of its constituent components. The Tafel slopes of  $\text{Co}_3\text{O}_4$ -FeOOH ( $94.92 \text{ mV dec}^{-1}$ ),  $\text{Co}_3\text{O}_4$  ( $123.3 \text{ mV dec}^{-1}$ ), and  $\text{FeOOH}$  ( $150.3 \text{ mV dec}^{-1}$ ) were obtained from the corresponding LSV curves. The results implies that the  $\text{H}_2$  production in our electrochemical system depending on the Volmer step ( $\text{H}_2\text{O} + e^- \rightarrow \text{H}_{ad} + \text{OH}^-$ ). The smaller Tafel slope of  $\text{Co}_3\text{O}_4$ -FeOOH compared with the other two samples indicates faster hydrogen adsorption on the heterojunction surface [88,89], confirming the accelerated HER kinetic of  $\text{Co}_3\text{O}_4$ -FeOOH (Fig. 5b). The EIS curves shown in Fig. 5c proves the faster charge transfer of  $\text{Co}_3\text{O}_4$ -FeOOH among all the samples prepared. These results suggest that the hetero-interface between  $\text{Co}_3\text{O}_4$  and  $\text{FeOOH}$  also plays a crucial role in hydrogen evolution. The durability test displayed in Fig. 5d demonstrates the good stability of the electrocatalyst towards the HER, with a well-maintained potential over 22 h, and shows almost no change in performance, as shown from LSV curves after the stability test (Fig. 5e), which illustrates the favorable HER activity of  $\text{Co}_3\text{O}_4$ -FeOOH.

Due to the excellent HzOR and HER performance, a two-electrode



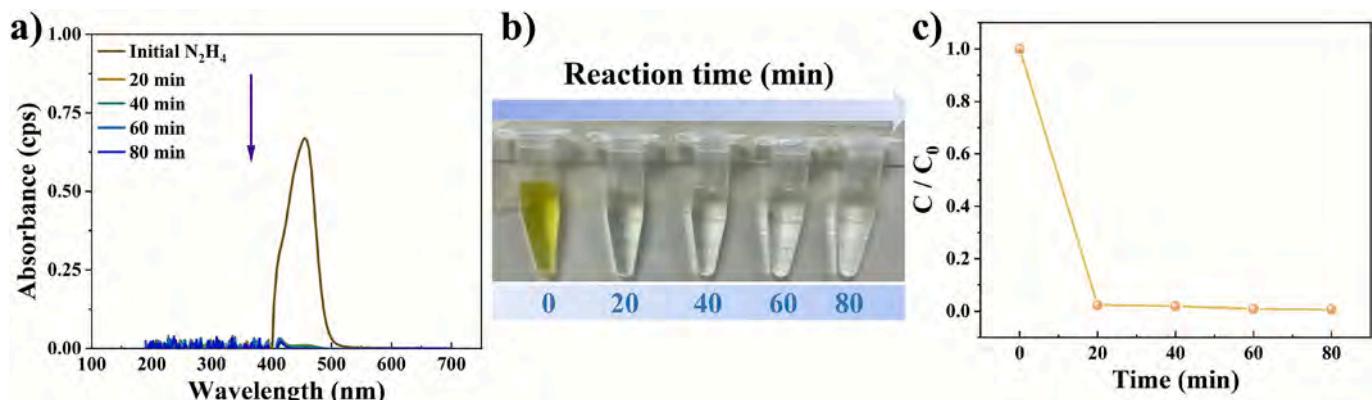
**Fig. 5.** a) Performances of  $\text{Co}_3\text{O}_4\text{-FeOOH}$ ,  $\text{Co}_3\text{O}_4$ , and  $\text{FeOOH}$  in HER; b) Tafel slopes extracted from a); c) EIS curves of  $\text{Co}_3\text{O}_4\text{-FeOOH}$ ,  $\text{Co}_3\text{O}_4$ , and  $\text{FeOOH}$  in HER; d) CP test of  $\text{Co}_3\text{O}_4\text{-FeOOH}$  in HER, and e) LSV curves of  $\text{Co}_3\text{O}_4\text{-FeOOH}$  before and after stability test; f) Performances of  $\text{Co}_3\text{O}_4\text{-FeOOH}$  in OHzs (1 M KOH + 0.5 M  $\text{N}_2\text{H}_4$ ), and OWS (1 M KOH).

cell was constructed to examine the electrocatalytic  $\text{H}_2$  production ability, with  $\text{Co}_3\text{O}_4\text{-FeOOH}$  being both anode and cathode. The LSV curves of overall water splitting (OWS) and overall hydrazine splitting (OHzs) were measured, as shown in Fig. 5f. A significant energy saving performance in OHzs was obtained, where only 0.49 V is required to deliver a current density of  $300 \text{ mA cm}^{-2}$ . In comparison, 1.95 V is required in OWS to achieve the same current density.

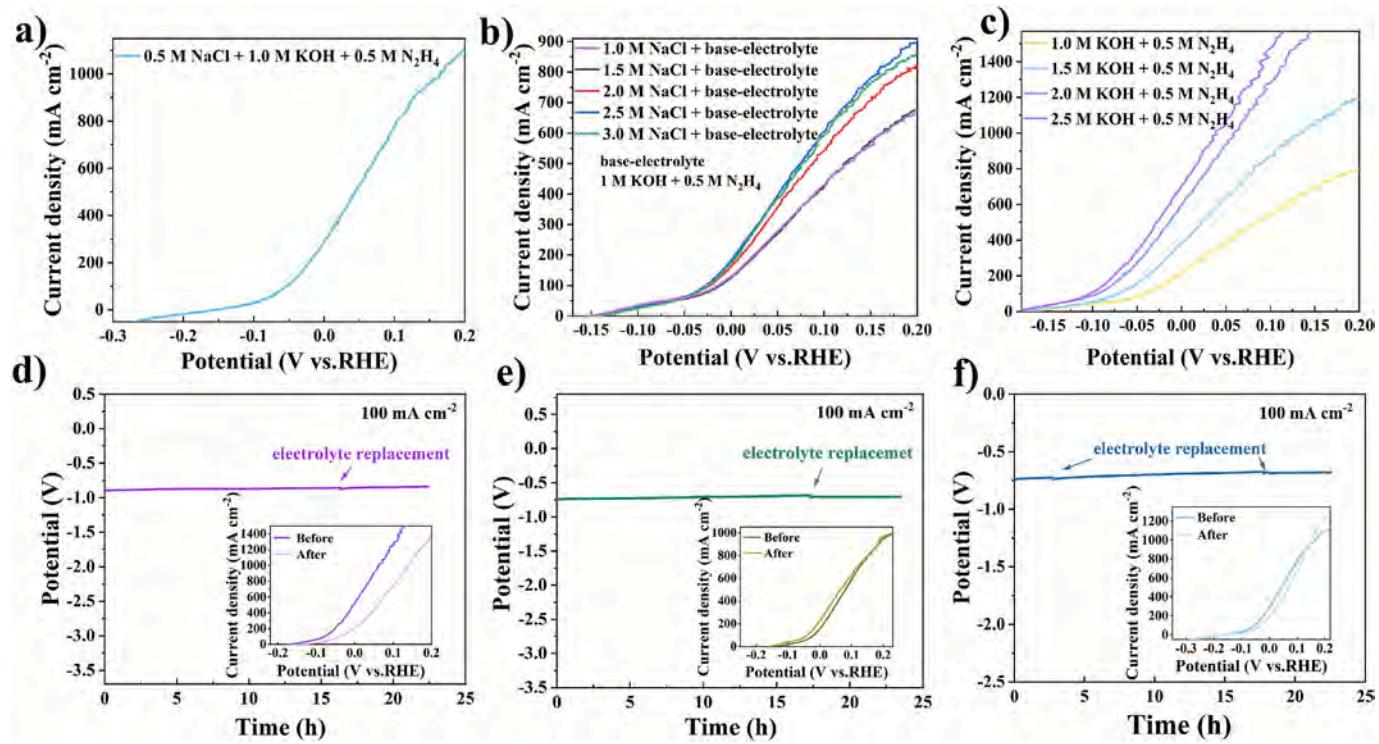
Hydrazine is a water pollutant that is highly toxic, carcinogenic, and poses serious health and environmental hazards. Therefore, achieving a high degradation rate in wastewater treatment is of great importance [90]. Coupling hydrogen production and hydrazine degradation can realize the ideal combination of high-efficiency hydrogen production and pollutant degradation with low energy consumption. Here, the Watt and Crisp method was employed to evaluate the  $\text{N}_2\text{H}_4$  degradation rate [91]. In short, equal volume of electrolyte was collected during the HzOR at a current density of  $100 \text{ mA cm}^{-2}$ . The residual hydrazine concentration was determined from the absorbance of the developed color, and the degradation rate was subsequently estimated. The results

showed that 100 mg / L of hydrazine was almost completely degraded after 20 min (Fig. 6), with a degradation rate of nearly 100 %, demonstrating a fast degradation rate and high efficiency. At the same time, the kinetics of the  $\text{N}_2\text{H}_4$  degradation process were investigated, as shown in Fig. S9. The high  $R^2$  value (0.9999) indicates the best fit, suggesting that the degradation of  $\text{N}_2\text{H}_4$  in this electrocatalytic system follows the BMG (Behnajady–Modirshahla–Ghanbery) kinetic model [92]. The result proves that it is possible to realize high hydrogen output and efficient hydrazine degradation with low energy consumption.

Given the excellent electrocatalytic performance of the  $\text{Co}_3\text{O}_4\text{-FeOOH}$  electrocatalyst, it is potentially applicable in various scenarios, such as seawater-coupled hydrogen production and other harsh environments, including highly alkaline solutions and alkaline brines. For hydrazine electrolysis, whether in simulated seawater (0.5 M NaCl + 1.0 M KOH), alkaline brine (2.5 M NaCl + 1.0 M KOH), or strong alkaline solution (2.5 M KOH),  $\text{Co}_3\text{O}_4\text{-FeOOH}$  exhibits remarkable electrocatalytic performance, as shown in Fig. 7, Figs. S10 and S11. Interestingly, the catalytic activity improves with increasing NaCl



**Fig. 6.** a) Evolution of UV-Vis absorption peak in OHzs; b) color change of the complex at different reaction times in the system; c) Hydrazine degradation rate in OHzs.



**Fig. 7.** LSV curves of  $\text{Co}_3\text{O}_4$ -FeOOH during HzOR in different system: a) simulated seawater; b) 1.0 M KOH + NaCl (1.0 M–3.0 M) + 0.5 M  $\text{N}_2\text{H}_4$ ; and c) KOH (1.0 M–2.5 M) + 0.5 M  $\text{N}_2\text{H}_4$ . CP curves and corresponding LSVs of  $\text{Co}_3\text{O}_4$ -FeOOH before and after the stability test in different systems: d) simulated seawater; e) 1.0 M KOH + NaCl (2.5 M) + 0.5 M  $\text{N}_2\text{H}_4$ ; and f) KOH (2.5 M) + 0.5 M  $\text{N}_2\text{H}_4$ .

concentration, probably due to enhanced solution conductivity. However, beyond a certain salt concentration (2.5 M NaCl), the performance enhancement was saturated. Similarly, increasing the KOH concentration also improves electrocatalytic performance, probably for a similar reason. Long-term stability tests in hydrazine-containing highly salty electrolytes (2.5 M NaCl + 0.5 M  $\text{N}_2\text{H}_4$  + 1 M KOH) and highly alkaline electrolytes (2.5 M KOH + 0.5 M  $\text{N}_2\text{H}_4$ ) confirm the catalyst's outstanding durability and electrochemical kinetics under high-salt and strong alkali conditions. Overall, the results demonstrate that the  $\text{Co}_3\text{O}_4$ -FeOOH electrocatalyst holds great promise for energy-saving hydrogen production and pollutant treatment.

#### 4. Conclusion

In summary, a  $\text{Co}_3\text{O}_4$ -FeOOH heterojunction electrocatalyst was successfully developed, significantly enhancing the electrocatalytic performance of the HzOR through the built-in electric field. Remarkably low potentials of -17.2 mV (vs. RHE) and 122.1 mV (vs.RHE) are required to achieve current densities of 100 and 400 mA cm<sup>-2</sup>, respectively, which are substantially lower than those needed for the OER to reach the same current densities. The HER performance of  $\text{Co}_3\text{O}_4$ -FeOOH has also shown improvement compared to the individual components. Furthermore, the catalyst's high activity facilitates energy-efficient hydrogen production in HzOR-coupled water electrolysis, achieving an impressively low potential of 0.49 V at a current density of 300 mA cm<sup>-2</sup> in OHzS. In comparison, conventional OWS demands a much higher potential of 1.95 V to reach the same current density, demonstrating significant energy savings. Beyond its excellent electrocatalytic performance in HzOR, the catalyst exhibits outstanding stability and activity under harsh conditions, such as simulated seawater, highly alkaline environments, and high-salinity media, highlighting its great potential in hydrogen production and pollutant treatment.

#### CRediT authorship contribution statement

**Liyuan Dai:** Writing – original draft, Software, Methodology, Investigation, Formal analysis, Data curation. **Yuta Tsuji:** Software, Writing – review & editing, Validation. **Hiroki Iwai:** Software, Validation, Writing – review & editing. **Quan Quan:** Validation, Writing – review & editing, Formal analysis. **Dongyuan Song:** Investigation, Data curation. **Xueda Liu:** Validation, Investigation. **Jiangyang Liu:** Investigation, Methodology, Writing – review & editing, Formal analysis. **Takeshi Yanagida:** Writing – review & editing, Supervision, Conceptualization. **Johnny C. Ho:** Writing – review & editing, Supervision, Resources, Methodology, Formal analysis, Conceptualization. **SenPo Yip:** Writing – review & editing, Resources, Methodology, Formal analysis, Conceptualization.

#### Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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## Appendix A. Supplementary data

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.apsusc.2025.165458>.

## Data availability

Data will be made available on request.

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